

PRODUCTION OF BIO-DIESEL FROM MICRO ALGAE GROWN IN WASTE WATER

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Abstract

The objective of this study is to evaluate the growth of micro algae *Chlorella protothecoides* in various percentage of waste water sampled from different terminals in batch culture. Evaluation of the growth of the micro algae along with the lipid production is estimated. Parameters such as in chemical oxygen demand, growth curve of the algae and variation in elements nitrogen and phosphorous is investigated by the growth of the algae in waste water. The media used is the basal media for the cultivation of the algae. Waste water from the domestic treatment plant in the campus is obtained from the terminals grid chamber (1), aeration tank (2) and from the secondary clarifier(3). The maximum growth is observed to be in the 50% waste water sampled from secondary clarifier with the biomass of 1.008g/l. It is also seen that there is efficient reduction in COD, nitrogen and phosphorous leading to the treatment of waste water along with the secretion of lipid of 19%. Hence the cultivation of *Chlorella protothecoides* can be adopted to grow in the waste water rich in nutrients that becomes economical as it do not require any fertilizers, media or fresh waters in specific for the bio diesel production without affecting the food chain of humans nor having any impact on the environment.

1. INTRODUCTION

There is a global shortage for the fossil fuels, specially oil and natural gas hence focus is over development of renewable bio fuel production. There is an immediate need to develop bio fuels because of depleting petroleum resources and increase in global energy demand. (Atefeh Ebrahimian, et al.,2014) Therefore the need for the bio fuel is the global issue as the fossil fuels are non renewable and unsustainable energy source. Additional cause for the focus on bio fuel is increase in the emission of large amount of carbon dioxide to the environment on burning the fossil fuels which has the tremendous effects on environment contributing to the green house effect. (Bharat Gamia et al.,2014)

Bio fuel is the one which serves as the alternative and renewable source for the fossil fuels. Therefore a major focus is over the production of bio fuels and has attracted attention over the production of bio diesel. There are various sources which form the feedstock for the bio diesel production like algae, vegetables, animal fats, jatropa seeds, rape seed, soybean, castor oil, neem seeds, jojoba oil etc.(Farooq Ahmad et al.,2013). Microalgae is considered as the potent stock for the bio diesel production as algae do not have any impact on the environment and non toxic and also do not harm the food chain despite vegetables. Microalgae requires large amount of water and nutrients for its growth which becomes ineffective for the cultivation. However it can also been grown in waste waters,(Sheng-Yi Chiu et al.,2015) sea waters which is rich in nutrients and salts which cuts the cost of cultivation conventionally. (Ashish Bhatnagar et al.,2011) Also on the other hand micro algae

require carbon dioxide for its growth which leads to carbon dioxide fixation that reduces the green house gases. Algal strains from genus of *chlorella* have the highest net bio mass accumulation is observed with *chlorella kessleri* followed by *chlorella protothecoides*.

Micro algae *Chlorella protothecoides* are the group of *chlorella* species that are mixotrophic that could be cultivated under autotrophic as well as heterotrophic conditions that utilize inorganic and organic substrates for its growth that leads to the synergistic effects of lipid production along with the treatment of waste water.(Fiona Lynch et al.,2015). This study is conducted to investigate the growth of *Chlorella protothecoides* in waste water of various percentages along with the basal media (Fatima Zahra Mennaa et al.,2015).. Also to study the amount of removal of COD, nitrogen and phosphorous in the waste water leading to the treatment of waste water simultaneously lipid accumulation and eventually bio diesel production.

2. MATERIALS AND METHODS

2.1 Algal culture and Waste Water Collection

Waste water is collected from the treatment plant in the campus at different terminals such as grit chamber, aeration chamber and from the secondary clarifier(Liang Wang et al.). The basal media is prepared according to the composition given in the table(1), in which the micro alga is grown. Waste water with the combination of media is made for different percentages of waste water like 25%, 50% , 75% and 100% waste water. *Chlorella protothecoides* is then inoculated into these combination of media – waste water as mentioned above. The samples were estimated for

the growth of the bio mass for every 24h and also analysed for the reduction in COD and nutrients nitrogen and phosphorous. From the data obtained the biomass growth curve was plot to see the adoption of microalgae to the various waste water samples prepared and studied the percentage of removal of the nutrients.

2.2 Lipid Extraction and Estimation

Blighdyer’s method is followed for the lipid extraction process. The bio mass obtained from the combinations of waste water samples as mentioned is estimated for the percentage of lipid accumulation. There are several methods for the lipid extraction process like solvent extraction, supercritical fluid extraction, ultrasonic extraction and mechanical pressing.

In this study lipid extraction is achieved by the solvent extraction method. A known quantity of bio mass is added to the solvent methanol: chloroform in the ratio 1:2 and vortex for about 10mins followed by the separation of biomass from the solvent. The solvent now consists of the lipid which is given a water wash to remove the water soluble impurities and other proteins. The phase is now separated from the water. To this lipid solvent extract the transesterification reaction is carried out using sulphuric acid as the catalyst. After the reaction is over the bio diesel produced during the reaction is extracted again into hexane.

3. RESULTS AND DISCUSSION

The investigation of growth curve of the *Chlorella protothecoides* depicted that the algae is well adopted to grow in all the combinations of waste water sample with varying growth curves. 50% waste water combination i.e 50%waste water: 50% media, showed the best results among the other combinations (25%, 50%, 75%,100% waste water). Sample from the secondary clarifier is observed to be the best suited for the algal growth with the maximum bio mass of 1.5008g/l. And lipid accumulation to be 19.36%, % of removal of nitrogen and phosphorous is 87.5% and 68.18% respectively in the waste water sample.

Biomass growth rate: samples of secondary clarifier.

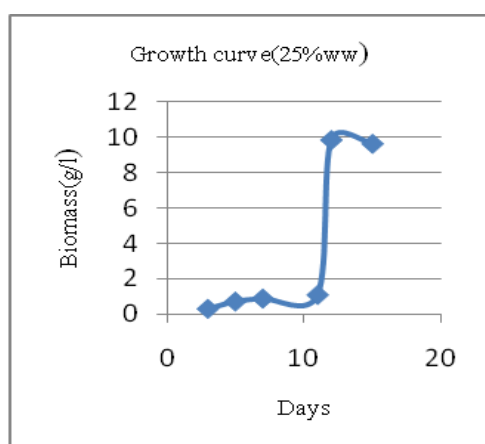


Fig 1: Showing the growth curve of 25% ww = 1.108 g/l

Table 1: The strain of *Chlorella protothecoides* is cultured in the basal media with composition as follows:

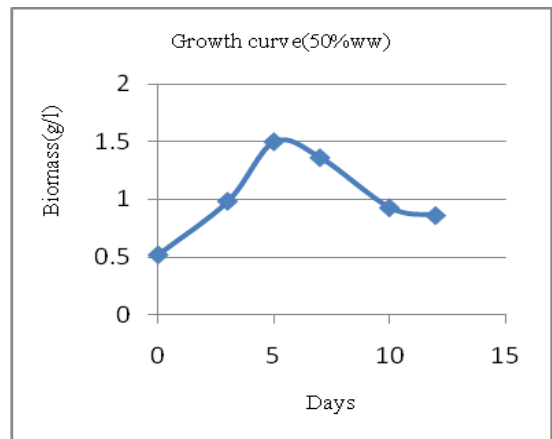


Fig 2 Showing the growth curve of 50% ww = 1.5008 g/l.

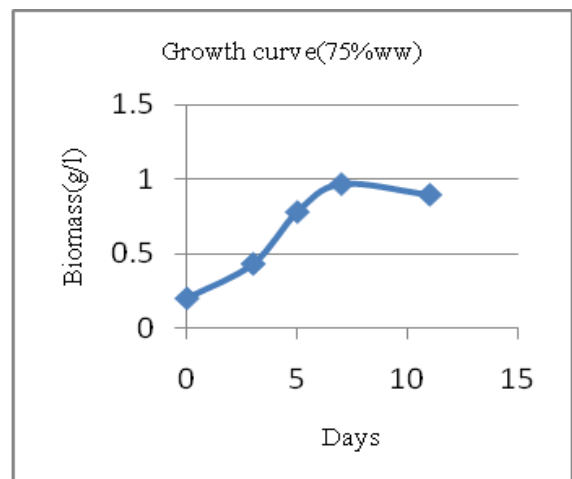


Fig 3 Showing the growth curve of 75% ww = 0.9647

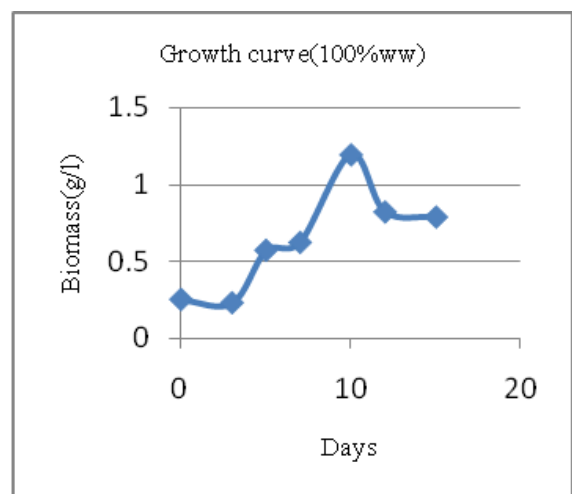


Fig 4 Showing the growth curve of 100% ww = 1.1926 g/l.

No.	Chemical	mg/l		Logarithmically growing cells	Late-logarithmically growing cells	Stationary phase cells
1	CO(NO ₃) ₂ .6H ₂ O	4.9	Initial dry cell weight concentration (X_0) [mg mL ⁻¹]	2.07	2.03	1.95
2	H ₃ BO ₃	114.2	Initial hydrogen production rate ($r_{H_2,0}$) [mmol mL ⁻¹ h ⁻¹]	0.025	0.031	0.027
3	ZnSO ₄ .7H ₂ O	88.2	Deactivation rate constant (k) [h ⁻¹]	0.017	0.019	0.006
4	EDTA	500	Number of moles of hydrogen per culture volume at 96 h ($y_{H_2,i}$) [mmol mL ⁻¹]	1.48	1.79	1.97
5	KH ₂ PO ₄	1250	Attainable number of moles of hydrogen per culture volume ($y_{H_2,f}$) [mmol mL ⁻¹]	1.86	2.18	4.24
6	FeSO ₄ .7H ₂ O	49.8	Specific death rate (K_d) [h ⁻¹]	0.00076	0.0011	0.0026
7	MgSO ₄ .7H ₂ O	1000	Number of moles of lactate per dry cell weight at 96 h [mmol mg ⁻¹]	0.0308	0.0323	0.188
8	KNO ₃	1250	Dry cell weight concentration at 96 h [mg mL ⁻¹]	1.95	1.86	1.49
9	CuSO ₄ .5H ₂ O	15.7	Lactate concentration at 96 h [mmol mL ⁻¹]	0.20	0.26	0.48
10	MnCl ₂ .4H ₂ O	14.2	Acetate concentration at 96 h [mmol mL ⁻¹]	0.05	0.21	0.80

Table 2: Results obtained from the grit chamber.

% of waste water	Biomass (g/l)	% of lipid Accumulation	COD (% of Reduction)	Nitrogen (% of Reduction)	Phosphorous (% of Reduction)
25	0.8096	7	38.86	90	18.39
50	1.3606	13.85	72.83	60	63.81
75	1.11	12.27	42.7	40	35.24
100	1.326	9.25	49.86	20	

Table 3: Results obtained from the aeration tank .

% of waste water	Biomass (g/l)	% of lipid Accumulation	COD (% of Reduction)	Nitrogen (% of Reduction)	Phosphorous (% of Reduction)
25	1.2506	11.2	47.85	10.81	26.67
50	1.316	16.34	65.23	37.79	60
75	1.2476	12.84	52.37	33.34	43.34
100	0.8436	10.06	42.09	40.48	64

Table 4: Results obtained from the secondary clarifier.

% of waste water	Biomass (g/l)	% of lipid Accumulation	COD (% of Reduction)	Nitrogen (% of Reduction)	Phosphorous (% of Reduction)
25	1.108	12.8	41.63	62.5	46
50	1.5008	19.36	76.93	81	68.2
75	0.9647	12.58	64.7	80	55.8
100	1.1926	14.67	60.04	84	46.22

Table (1) shows the result table of grit chamber, table (2) shows the result for the sample from aeration tank, table (3)

shows the result table for the sample from the secondary clarifier., indicating biomass growth, % of lipid

accumulation, % of COD reduction and elements such as phosphorous and nitrogen removal.

4. PRODUCTION OF BIODIESEL

As is evident from table (2) ,(3), and (4)..., optimum condition for lipid and biomass concentration were: sample from secondary clarifier of 50% waste water combination. The alga was grown under these condition in 100l open pond. The lipids were extracted using chloroform : methanol (2:1) and subjected to acid catalyzed esterification in lab scale reactor. Different concentrations of methanol and H₂SO₄ were used as depicted in the table. In a given run, lipid were transferred to reactor along with H₂SO₄ and methanol. The temperature was set at 65°C and the contents stirred for 1.5h. after the reaction hexane was added in the ratio of 0.2ml hexane/ml of reaction mixture and stirred at 500rpm in a magnetic stirrer. Following mixing, the contents were transferred to separating funnel. The upper hexane phase containing FAME (biodiesel) was separated and hexane was separated by rotovac. The weight of biodiesel produced was noted and yield was calculated as ,

$$\text{Yield of biodiesel}(\text{g biodiesel/g lipid}) = \frac{\text{g of FAME produced}}{\text{g of lipid used}} * 100$$

Table 5: amount of lipids used = 1g, temperature = 65°C

Weight ratio of methanol to lipid	Yield of biodiesel
20:1	72.3
30:1	76.5
40:1	81.3
50:1	88.6
60:1	92.6
70:1	90.3
80:1	87.3

As can be seen from table (5) optimum conditions for biodiesel production were: wt ratio of methanol : lipid = 60:1.

5. CONCLUSION

Comparing the results from table (2), (3) and (4) it is clear that secondary clarifier with 50% waste water combination shows the best results with the maximum biomass accumulation of 1.5008g/l and highest lipid accumulation with 19.36%.

Using waste water as the medium for the growth of microalgae can reduce the capital cost, land required on the treatment of waste water and also over the bio diesel production plant setup. Micro algae has shown good growth in the waste water medium with the synergistic effect of treatment by the removal of the elements phosphorous, nitrogen and COD present in the effluents. It also cuts down the cost of chemicals used for the medium to grow the micro algae for the production of biodiesel.

Major focus is over the methods of harvesting of micro algae and the extraction of lipids which involves large amount of solvent. The growth of micro algae is also efficient in secreting the lipids that is grown in primary and secondary waste water.

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